



## Full Length Article

Smoldering peat fire detection by time-resolved measurements of transient CO<sub>2</sub> and CH<sub>4</sub> emissions using a novel dual-gas optical sensorMohsin Raza<sup>a,1</sup>, Yuying Chen<sup>b,1</sup>, Joshua Trapp<sup>a</sup>, Haojia Sun<sup>a</sup>, Xinyan Huang<sup>b,\*</sup>, Wei Ren<sup>a,\*</sup><sup>a</sup> Department of Mechanical and Automation Engineering, and Shenzhen Research Institute, The Chinese University of Hong Kong, New Territories, Hong Kong SAR, China<sup>b</sup> Research Centre for Fire Safety Engineering, Department of Building Environment and Energy Engineering, The Hong Kong Polytechnic University, Hong Kong SAR, China

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## ABSTRACT

A compact and sensitive dual-gas laser absorption sensor was developed for smoldering peat fire detection by real-time monitoring of transient CO<sub>2</sub> and CH<sub>4</sub> emissions from peat combustion exhaust. The sensor combines two infrared lasers to exploit CH<sub>4</sub> and CO<sub>2</sub> absorption lines centered at 6057.09 cm<sup>-1</sup> and 6359.96 cm<sup>-1</sup>, respectively. Scanned-wavelength modulation spectroscopy with the second-harmonic detection (WMS-2f) and a custom-designed Herriot multipass gas cell (10.3 m path length in a 40.5 mL volume) were employed to improve detection sensitivity. The simultaneous real-time transient emissions (CH<sub>4</sub> and CO<sub>2</sub>) were measured at an interval of 0.1 s under various smoldering peat combustion conditions in a top open cylindrical reactor. An increasing trend of CH<sub>4</sub>/CO<sub>2</sub> ratio from 0.053 to 0.075 and the greenhouse gas (GHG) flux from 1.5 g/m<sup>2</sup> s to 3.4 g/m<sup>2</sup> s was observed with increasing oxygen supplies from 10 mm/s to 24 mm/s. However, a decreasing trend of CH<sub>4</sub>/CO<sub>2</sub> ratio from 0.06 to 0.043 and GHG flux from 2.6 g/m<sup>2</sup> s to 0.4 g/m<sup>2</sup> s was noticed with increasing peat moisture content from 8% (dry peat) to 100%. The measurement results agree well with commercial non-dispersive infrared CO<sub>2</sub> and CH<sub>4</sub> analyzers which are not fast enough to capture transient emissions due to their low time response. The developed dual-gas sensor has the potential to be applied for detecting underground peatland fires and evaluating the overall GHGs emissions from smoldering wildfires due to its excellent temporal resolution, hardware simplicity, and compactness.

## 1. Introduction

Smoldering is the slow, low-temperature, and flameless burning of porous fuels and one of the most persistent types of combustion phenomena [1]. Smoldering peat fires are the largest wildfires on Earth (in terms of fuel consumption) that irreparably degrade soil ecosystems [2]. The global smoldering peat fires release massive greenhouse gases (GHGs), mainly carbon dioxide (CO<sub>2</sub>) and methane (CH<sub>4</sub>) as reported in the literature [3–5], which is equivalent to 10–15% of man-made emissions and comparable to the total emissions from the European Union [6,7]. Measuring the concentrations of these two primary GHGs (CH<sub>4</sub> and CO<sub>2</sub>), as well as their ratio, can help detect smoldering peat fires and estimate fire intensity. Compared to flaming wildfires [3,8], smoldering wildfires generate more unburnt hydrocarbons and toxic gases [9,10], but relatively few studies focus on the dynamic emissions

from smoldering. This work aims to develop new methods and sensors for detecting smoldering peat fires by measuring transient CO<sub>2</sub> and CH<sub>4</sub> emissions, which helps pave the way for studying real peatland fires.

Several commercially available instruments including metal oxide semiconductor sensors, non-dispersive infrared (NDIR) sensors, gas chromatography-mass spectrometry (GC-MS), and Fourier transform infrared (FTIR) spectroscopy have been used for CH<sub>4</sub> and CO<sub>2</sub> monitoring in combustion systems and process industrial units. Metal oxide semiconductor gas sensors are compact, lightweight, and offer a quick response time (<1 min), and high sensitivity (ppm-level), but they need a high temperature for operation and their performance is affected by humidity [11]. NDIR sensors have been widely used for monitoring GHGs emissions [12–15], but they suffer from low sensitivity, poor selectivity, and instability [16]. GC-MS and FTIR have been used for analyzing smoldering combustion emissions [17–19]. GC-MS can be

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used to analyze complex gas mixtures due to its advantages of temporal separation of molecules [20]. However, it reduces the possibility of real-time measurements due to the long analysis time up to tens of minutes required for the gas mixture to be separated in the capillary column [21]. Furthermore, the high cost, bulky size, and heavy weight limit its wide applications. FTIR spectrometer has been employed for multi-component analysis with a wide spectral coverage [22], but it suffers from slow response time, high cost, and bulky size.

Tunable diode laser absorption spectroscopy (TDLAS) is a powerful trace gas sensing technology compared to the above-mentioned methods, which offer highly sensitive, accurate, quantitative, and species-specific measurements as well as robust and compact sensor systems [23–25]. The advantage of short response time makes it particularly suitable for online real-time gas process control and combustion exhaust monitoring applications. TDLAS sensors have been widely used for GHG sensing and exhaust gas monitoring in industrial combustion systems. However, their applications for smoldering combustion research have been scarcely reported. Hangauer et al. developed a 2.3  $\mu\text{m}$  CO sensor using vertical-cavity surface-emitting lasers (VCSELs) for smoldering wood fire detection [26]. They achieved sub-ppm level of CO detection with a time resolution of 1 min. Fallows et al. demonstrated a portable cavity ringdown spectrometer for detecting smoldering cigarettes fire [27], and successfully detected a peak concentration of 270 ppm CO, 2100 ppm CO<sub>2</sub>, and 310 ppb C<sub>2</sub>H<sub>2</sub>.

Smoldering cigarette fire has also been detected by measuring nitric oxide (NO) using a 5.24  $\mu\text{m}$  quantum cascade laser (QCL) [28]. The detection limit of 28 ppb over 180 s integration time was achieved using a single-pass absorption cell with an effective path length of 1 m. Qiu et al. demonstrated a 2.3  $\mu\text{m}$  distributed feedback laser-based CO sensor for smoldering fire detection using scanned-WMS combined with a Herriot-type multipass cell (19.98 m effective path length) [29]. The above literature reveals that earlier research studies have not reported the smoldering peat fire detection by measuring emission gases with the state-of-the-art TDLAS-based sensors. Hence, their potential for smoldering combustion and wildfires is valuable to be explored.

In this work, a compact and sensitive dual-gas sensor was designed based on time-division multiplexed scanned-WMS-2f for detecting peat fire by real-time monitoring of transient CH<sub>4</sub> and CO<sub>2</sub> in the smoldering peat combustion exhaust. The developed sensor can simultaneously detect CH<sub>4</sub> and CO<sub>2</sub> by targeting the selected lines peaked at 6057.09  $\text{cm}^{-1}$  and 6359.9  $\text{cm}^{-1}$ , respectively. These transition lines present in the near-infrared region have relatively weak absorption strength compared to strong absorption lines in the mid-infrared region [30,31]. However, the current mid-infrared laser sources are not widely used for field applications due to their high cost. To obtain a higher detection sensitivity using the near-infrared lasers, a custom-designed multipass gas cell (effective path length greater than 10 m in a 40.5 mL volume) was employed for developing a highly sensitive and inexpensive dual gas detector. The sensor performance was evaluated in terms of its stability, measurement precision, and detection limit in the laboratory. The developed sensor was applied for real-time monitoring of CH<sub>4</sub> and CO<sub>2</sub> from the exhaust of a lab-scale smoldering combustion reactor.

## 2. Time-division multiplexing laser absorption spectroscopy

The principle of laser-based absorption spectroscopy has been comprehensively explained previously [32], thus a brief description is presented here to establish notation. The foundation of laser absorption spectroscopy is the Beer-Lambert relation which relates the interaction of monochromatic light and uniform gas-phase atoms or molecules as described in Eq (1):

$$\tau(\nu) = (I_t/I_0)_\nu = \exp(-\alpha_\nu) = \exp(-S(T)\phi_\nu XPL) \quad (1)$$

where incident and transmitted laser intensities are represented by  $I_0$  and  $I_t$ , respectively,  $\alpha_\nu$  is the spectral absorbance,  $\phi_\nu$  refers to the line-

shape function,  $S(T)$  ( $\text{cm}^{-2} \text{atm}^{-1}$ ) is the line-strength of the transition at temperature  $T$  (K),  $X$ ,  $L$ , and  $P$  represents the mole fraction, optical path length, and total gas pressure, respectively.

Scanned-WMS-2f detection scheme is preferred for trace gas detection with a relatively small amount of absorbance [23]. The nominal wavelength of a tunable diode laser is usually scanned across the absorption line of the target species with a slow (Hz) sawtooth or triangular injection current. An additional sinusoidal modulation at fast (kHz) frequency  $f$  applies to the slower scan current. The laser output frequency can be described by Eq. (2):

$$\nu(t) = \bar{\nu} + a \cos(2\pi ft) \quad (2)$$

where  $\bar{\nu}$  ( $\text{cm}^{-1}$ ) is the laser-center frequency and  $a$  ( $\text{cm}^{-1}$ ) is the modulation depth. The laser intensity  $I_0$  is modulated simultaneously while tuning the laser injection current:

$$I_0(t) = \bar{I}_0 [1 + i_1 \cos(2\pi ft + \psi_1) + i_2 \cos(2\pi ft + \psi_2)] \quad (3)$$

where  $\bar{I}_0$  is the average laser intensity,  $i_1$  and  $i_2$  are the linear and nonlinear laser intensity modulation amplitudes, respectively;  $\psi_1$  and  $\psi_2$  are the linear and nonlinear phase shifts between the laser intensity modulation and wavelength modulation. As the laser output frequency  $\nu$  is modulated, the fractional transmission  $\tau$  as a function of  $\nu$  becomes a periodic function at  $f$ . Thus, the transmitted laser intensity measured by the detector can be expanded by a Fourier series:

$$I_t(t) = I_0(t) \cdot \tau(\nu(t)) \\ = \bar{I}_0 [1 + i_1 \cos(2\pi ft + \psi_1 f) + i_2 \cos(2\pi ft + \psi_2 f)] \cdot \left[ \sum_{k=0}^{\infty} H_k \cos(k \cdot 2\pi ft) \right] \quad (4)$$

where  $H_k$  is the  $k$ th order Fourier harmonic coefficient that contains the absorption information [33]. Under the optical-thin condition,  $H_k$  is linearly proportional to the gas concentration. Thus, the target gas concentration can be derived from the measured harmonic signal if other properties of the target gas are known.

In the scanned-WMS-2f scheme, high-frequency modulation is added in the laser injection current to raise the signal detection band to the designated higher frequency range, which eliminates the low-frequency noise in practical measurements and thus significantly increases the signal-to-noise ratio (SNR). A lock-in amplifier (LIA) is used to extract the 2f component which multiplies the measured photodetector laser intensity signal with the reference sinusoid at 2f and shifts the harmonic component to DC. Then a low-pass filter is employed to isolate the DC signal and reject other noise beyond the filter passband. Therefore, the scanned-WMS-2f technique usually merits a larger SNR under noisy environmental conditions and is particularly suitable for trace gas sensing in the field.

Time-division multiplexing (TDM) is an effective method used for multispecies gas sensing due to its advantages of simpler hardware and data processing [34]. In the TDM-WMS technique, each laser is switched on in succession, resulting in a detector signal that is composed of each laser signal in sequence. Both lasers are modulated at different modulation frequencies but scanned at the same scanning frequency to target the absorption lines. A sequence chart of an individual (1572 nm CO<sub>2</sub> laser, 1654 nm CH<sub>4</sub> laser) and combined time-division multiplexed dual-lasers WMS signal is shown in Fig. 1. In this work, the selected CO<sub>2</sub> and CH<sub>4</sub> absorption transitions were exploited by scanning the laser's wavelength at 10 Hz along with fast sinusoidal modulation frequencies of 15 kHz and 18 kHz, respectively. The measurements were completed every 200 ms by activating lasers in turn of 100 ms. One photodetector was used to record absorption signals and then pass through digital lock-in amplifiers to obtain the second harmonic WMS (WMS-2f) signals.

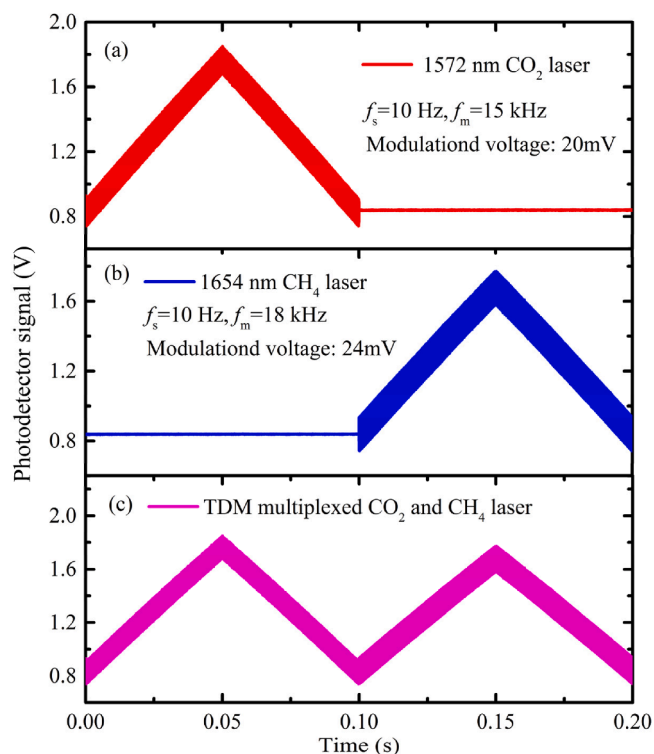


Fig. 1. Sequence chart of measured photodetector signals for (a) CO<sub>2</sub> at 1572 nm, (b) CH<sub>4</sub> at 1654 nm, and (c) combined time-division multiplexed dual-laser.

### 3. Experimental methods

#### 3.1. Absorption line selection

The performance and accuracy of laser absorption sensors can be significantly improved by carefully selecting the absorption line. In Fig. 2, the line strength is shown in the near-infrared range of 5603–6059 cm<sup>-1</sup> for CH<sub>4</sub> and 6350–6420 cm<sup>-1</sup> for CO<sub>2</sub>. The spectral lines of 6057.09 cm<sup>-1</sup> for CH<sub>4</sub> and 6359.9 cm<sup>-1</sup> for CO<sub>2</sub> were chosen due to their strong absorption, spectral isolation from the nearby transitions, and coverage within a single laser scan range. Two NIR distributed feedback diode lasers (1650 nm for CH<sub>4</sub> and 1572 nm for CO<sub>2</sub>) were employed to target the selected absorption lines. A spectrum analyzer

(Bristol Instruments) was utilized to characterize both lasers. The linear relation between the laser injection current and wavenumber is shown in Fig. 2. The 1650 nm DFB laser was scanned across the target CH<sub>4</sub> line by changing the laser current between 40 and 100 mA at 27 °C laser temperature while the 1572 nm laser exploited the CO<sub>2</sub> line by setting the laser temperature to 25 °C and varying the injection current between 35 and 95 mA.

#### 3.2. Sensor system configuration

Fig. 3 (a) depicts the dual-gas sensor system comprised of two near-infrared distributed feedback (DFB) diode lasers with 14-pin butterfly packages (Wuhan Liujiu ltd.), low-noise laser drivers (Wavelength Electronics ltd.), a custom-made multipass gas cell (MGC), and gas-handling equipment. A LabVIEW-based function generator was used to control both laser's modulation currents. The transmitted laser intensity signal was transformed from the time domain to the frequency domain using a silicon etalon with a free spectral range of 0.0834 cm<sup>-1</sup>.

In this work, a customized mini-Herriot-type MGC with a 10.3 m path length in a 40.5 mL volume was employed. It was composed of two 1-inch diameter spherical mirrors. The spherical concave mirrors were designed by using Zemax software as explained in Ruyue et al. [36]. A wavelength beam combiner was used to combine both CH<sub>4</sub> (1650 nm) and CO<sub>2</sub> (1572 nm) laser beams. The seven nonintersecting-circle spot patterns on both mirrors was accomplished by coupling the combined laser beam into the MGC as illustrated in Fig. 3 (a). The laser beam exiting the MGC was focused on an infrared photodetector (PDA20CS2, Thorlabs) by a 50 mm focal lens.

The gas-handling system, which included mass flow controllers, a mixing tank, and compressed CO<sub>2</sub>, CH<sub>4</sub>, and N<sub>2</sub> gas cylinders, was connected to the mini-MGC to calibrate the dual-gas sensor. Mass flow controllers were used to control the flow rate of the target gases, which were mixed in a tank and then filled into the cell for measurements.

#### 3.3. Lab-scale smoldering fire test

Peat soil was chosen as a representative fuel that is prone to smoldering combustion. Before the test, the peat sample was oven-dried at 90 °C for 48 h. The bulk density of the dried peat sample was measured to be 145 ± 10 kg/m<sup>3</sup>. The proximate analysis shows 70.8%, 23.5%, and 5.7% mass fractions for volatile matters, fixed carbon, and ash, respectively. The element analysis of the wood sample shows 46.09%, 5.75%, 47.46%, 0.47%, and 0.23% mass fractions for C, H, O, N, and S, respectively. To obtain different moisture contents, the dried peat was then well mixed with the corresponding amount of water. The schematic

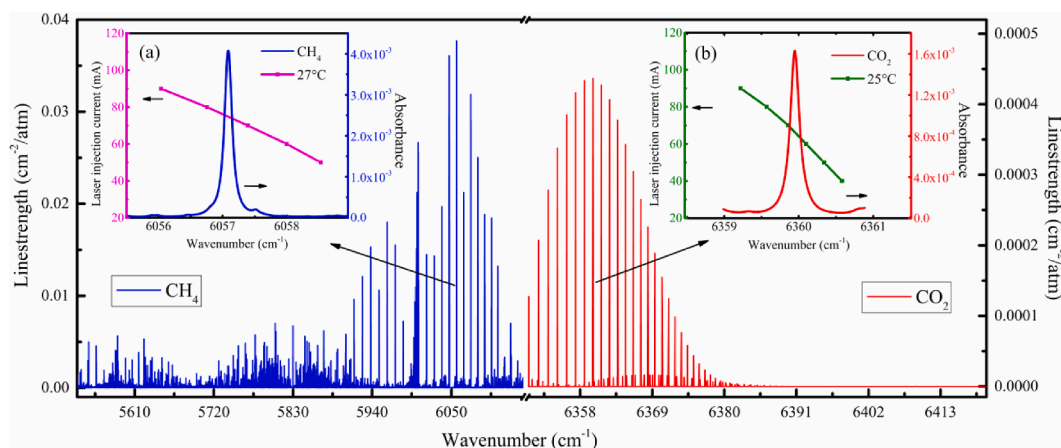
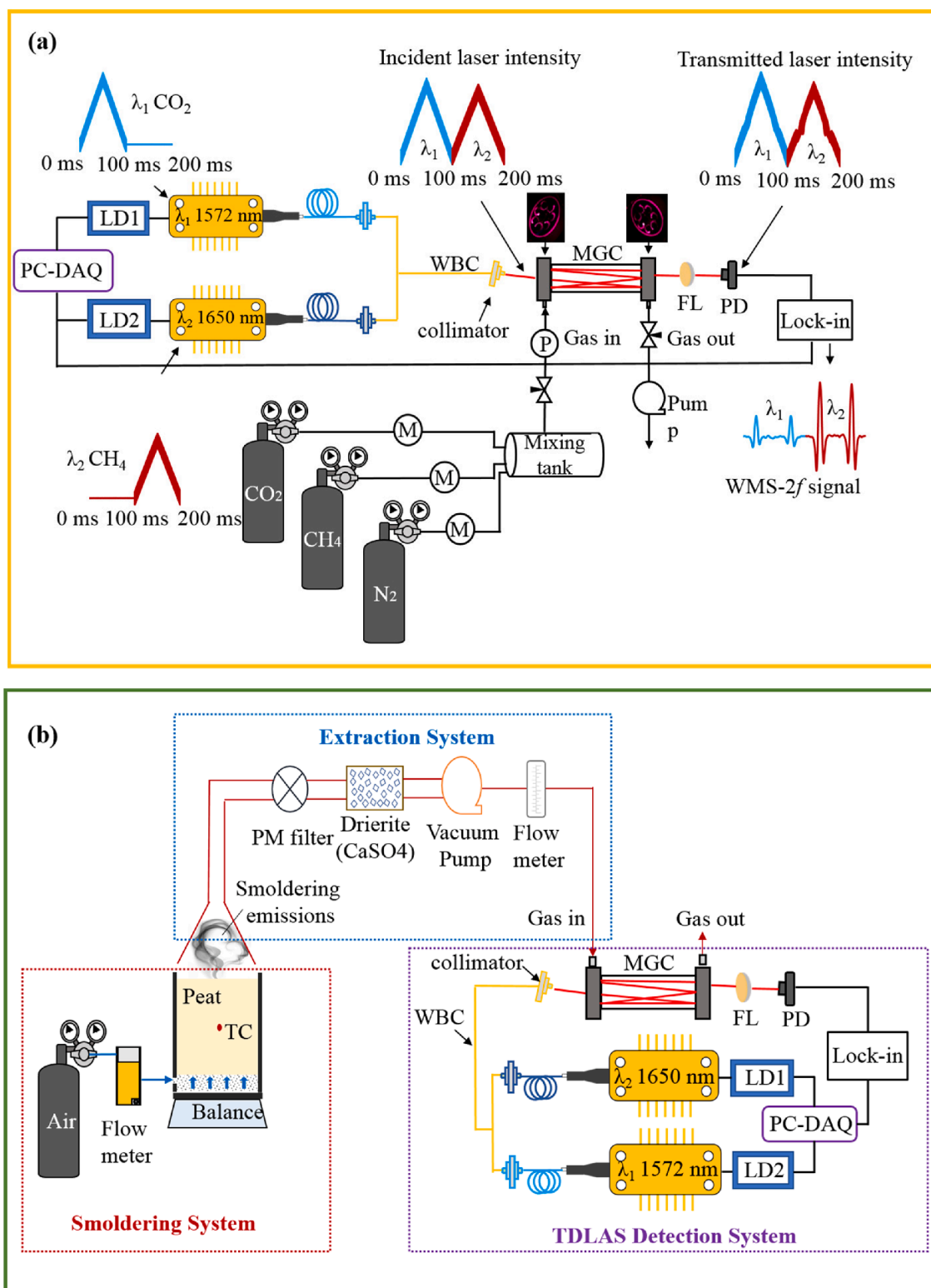


Fig. 2. Spectral line strength in the near-infrared range of 5603–6059 cm<sup>-1</sup> for CH<sub>4</sub> and 6350–6420 cm<sup>-1</sup> for CO<sub>2</sub> (HITRAN database) [35]. Inset graphs: wave-number variation of (a) 1650 nm laser and (b) 1572 nm laser with the laser injection current, along with the simulated absorption spectra of 9 ppm CH<sub>4</sub> and 850 ppm CO<sub>2</sub> at 1 atm, 300 K, and an absorption length of 10.3 m.



**Fig. 3.** (a) Schematic of the dual-gas (CH<sub>4</sub> and CO<sub>2</sub>) sensor system. PD: photodetector; LD: laser driver; WBC: wavelength beam combiner; P: pressure sensor; M: mass flow controller; FL: focusing lens; MGC: multipass gas cell. (b) Schematic diagram of the experimental setup for the time-resolved laser absorption measurements of CO<sub>2</sub> and CH<sub>4</sub> in smoldering combustion exhaust.

diagram of the experimental setup for time-resolved laser absorption measurements of CO<sub>2</sub> and CH<sub>4</sub> in smoldering combustion exhaust is shown in Fig. 3 (b). It includes a smoldering system, an extraction system, and the TDLAS detection system. The smoldering system consists of a small top-open cylindrical reactor and forced air supply devices. A

sample with a controlled volume was filled into the reactor with a height of 10 cm. A forced airflow was supplied from the bottom of the reactor, and the flow rate was controlled by the flow meter. To monitor the smoldering temperature, a K-type thermocouple was inserted into the fuel sample with its bead at the center of the reactor. The electrical



balance (PS 10100.R2, RADWAG) with a maximum measuring range of 10100 g and a precision of 0.01 g was used for weighing the mass loss of the peat during smoldering combustion.

The smoldering combustion was initiated by the lighter with a flame for 2 min, which was strong enough to generate a robust smoldering. A forced airflow was supplied after ignition. We controlled two parameters in the smoldering system such as the airflow velocity ( $u_{air} = 10$  mm/s, 18 mm/s, and 24 mm/s) and the peat moisture content (MC = 8%, 50% and 100%). After the successful smoldering combustion, the smoldering exhaust gases were extracted from above the burner by a pump and entered into the MGC at a flow rate of 600 mL/min after filtering the particulate matter (PM) and drying the smoldering emissions. The transient CH<sub>4</sub> and CO<sub>2</sub> emissions were simultaneously detected by our developed TDLAS sensor.

## 4. Results and discussion

### 4.1. Sensor performance evaluation

In WMS measurements, the 2f-signal depends not only on line parameters such as line strength but also on the modulation depth ( $a$ ). The optimum modulation depth needs to be selected to obtain the maximum amplitude of the 2f-signal. In this test, the gas mixture of 1170 ppm CH<sub>4</sub> and 11.05% CO<sub>2</sub> was filled in the MGC to measure the WMS-2f amplitude at different modulation depths by varying applied modulation voltages to 1650 nm laser and 1572 nm laser. The maximum amplitude 2f-signal for CH<sub>4</sub> and CO<sub>2</sub> was found at an optimum modulation depth of 24 mV and 20 mV, respectively, as shown in Fig. 4.

The developed dual gas sensor was first tested and calibrated in the laboratory at atmospheric pressure and room temperature. The WMS-2f signals of CH<sub>4</sub> and CO<sub>2</sub> with known concentrations are shown in Fig. 5 (a) and (b). The WMS-2f amplitude peak of measured signals as a function of known gas concentrations is plotted as a linear relationship in Fig. 5 (c) for CH<sub>4</sub> and (d) for CO<sub>2</sub>. The continuous monitoring of the peak amplitude of the WMS-2f signal for each tested gas concentration is shown in the inset of Fig. 5 (c) for CH<sub>4</sub> and (d) for CO<sub>2</sub>.

Allan-Werle deviation analysis was used to determine the sensor minimum detection limit (MDL) by measuring pure N<sub>2</sub>. The continuous measurement was conducted for ~ 15 min by scanning the time-division multiplexed CH<sub>4</sub> laser (1650 nm) and CO<sub>2</sub> laser (1572 nm) across the target absorption lines at a 10 Hz rate. The results of Allan-Werle deviation analysis are plotted in Fig. 6 (a) for CH<sub>4</sub> and Fig. 6 (b) for CO<sub>2</sub>, respectively. The MDLs of 0.82 ppm-CH<sub>4</sub> and 220 ppm-CO<sub>2</sub> were attained at 0.05-s integration time, which was then enhanced to 0.058 ppm-CH<sub>4</sub> and 17 ppm-CO<sub>2</sub> at 42-s and 27-s integration time, respectively.

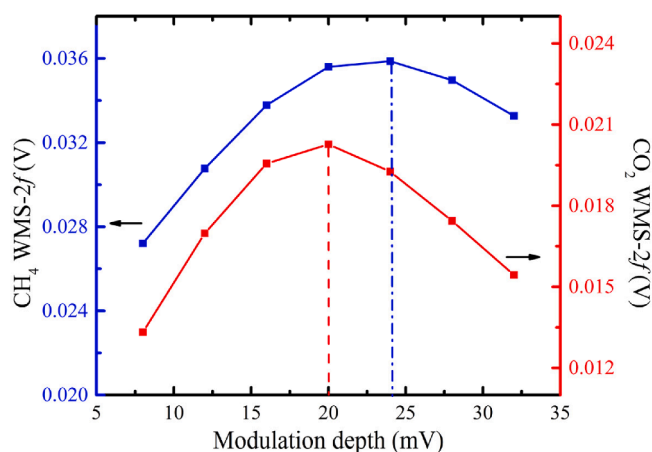


Fig. 4. Measured amplitude of 2f signal versus modulation depth for 1170 ppm CH<sub>4</sub> and 11.05% CO<sub>2</sub> gas mixture.

The sensor stability and precision were examined by recording the continuous time-series measurements of 9 ppm CH<sub>4</sub> and 850 ppm CO<sub>2</sub> gas mixtures as shown in Fig. 7 (a) and (b), respectively. Noise sources such as laser instability, temperature change, and mechanical vibration can influence the sensor system stability [37]. The continuous concentration measurements were recorded to evaluate the random noise level of optical measurement as shown in Fig. 7 (a) which indicates that the sensor system has good stability with little drift caused by the random noise. The frequency distributions of the continuous measurements of CH<sub>4</sub> and CO<sub>2</sub> are presented in the histogram plot in Fig. 7 (c) and (d), respectively. The measured concentration distributions of CH<sub>4</sub> and CO<sub>2</sub> can be fitted by the Gaussian profile. The half-width at half maximum (HWHM) of the Gaussian profile is determined to be 0.52 ppm for CH<sub>4</sub> and 56 ppm CO<sub>2</sub>, corresponding to a precision of 5.4% ( $9 \pm 0.52$  ppm) and 6.1% ( $850 \pm 56$  ppm) at 0.1 s average time, respectively.

The uncertainties in CH<sub>4</sub> and CO<sub>2</sub> measurements were estimated to be 6.21% and 6.22%, respectively, by taking into account the optical measurement uncertainty of 5.4% for CH<sub>4</sub> and 6.1% for CO<sub>2</sub>, uncertainty of the thermal-type MFC (0.7%), and line-strength uncertainty of CH<sub>4</sub> (3%) and CO<sub>2</sub> (1%) from the HITRAN database.

### 4.2. Smoldering emission monitoring

The performance of the TDLAS sensor was compared with the traditional commercial instruments (NDIR CO<sub>2</sub> and CH<sub>4</sub> analyzers, TSI Ltd.) by conducting real-time measurements of the smoldering emissions under the airflow velocity of 10 mm/s. As shown in Fig. 8, the continuous time-series measurement results of our developed TDLAS sensor were found to be in good agreement with commercial detectors. It was noticed that the commercial NDIR CO<sub>2</sub> and CH<sub>4</sub> analyzers show a time resolution of ~ 2.5 min and ~ 3 min, respectively, which is inadequate for measuring the transient change in emission gas concentration. Additionally, these detectors were not able to detect gas concentrations below 10 ppm. However, our developed TDLAS sensor offers a quick response with a time resolution of 0.1 s. Besides, the TDLAS sensor can easily detect very low gas emissions at a few ppm levels.

As oxygen supply and fuel moisture content are two important parameters influencing smoldering combustion, we used the developed TDLAS sensor to detect the smoldering emissions under various airflow velocities and peat moisture contents. Fig. 9 shows the evolutions of the mass-loss rate, and CO<sub>2</sub> and CH<sub>4</sub> concentrations during the smoldering combustion. It should be noted that the data recording starts when the airflow is turned on, thus the ignition period is not included. As shown in Fig. 9, the evolution of the CO<sub>2</sub> and CH<sub>4</sub> concentrations follow the trend of mass loss rate of peat smoldering, indicating that the gas emissions are dependent on the oxygen supply and combustion dynamics. When the airflow velocity increases from 10 to 18 mm/s, both CO<sub>2</sub> and CH<sub>4</sub> concentrations show significant increases, which is due to the intense smoldering reaction under the enhanced oxygen supply. However, as the airflow velocity continuously increases from 18 mm/s to 24 mm/s, the CO<sub>2</sub> and CH<sub>4</sub> emissions decrease slightly instead, which agrees with the variation of the mass-loss rate. This may be caused by the non-negligible convective heat loss under an excessively large airflow of 24 mm/s. In other words, the smoldering reaction is more intense under the airflow velocity of 18 mm/s which can be verified from the larger mass loss rate in Fig. 9a, thus, causing more gas emissions to be released.

It is also observed that the CO<sub>2</sub> concentration is significantly larger than that of CH<sub>4</sub>. Additionally, CO<sub>2</sub> is emitted for a slightly longer period than CH<sub>4</sub>. In other words, when the CH<sub>4</sub> concentration decreases to 0 ppm, the CO<sub>2</sub> concentration is still very large at the same moment. This is because CH<sub>4</sub> is mainly produced from peat pyrolysis, and this reaction is weakened after the smoldering front reaches the bottom of the reactor. In contrast, CO<sub>2</sub> is mainly emitted from char oxidation which still exists based on the fact that the mass-loss rates in Fig. 9(a) are still larger than 1 g/min.

Fig. 10 shows the CH<sub>4</sub> and CO<sub>2</sub> emissions measured by TDLAS under

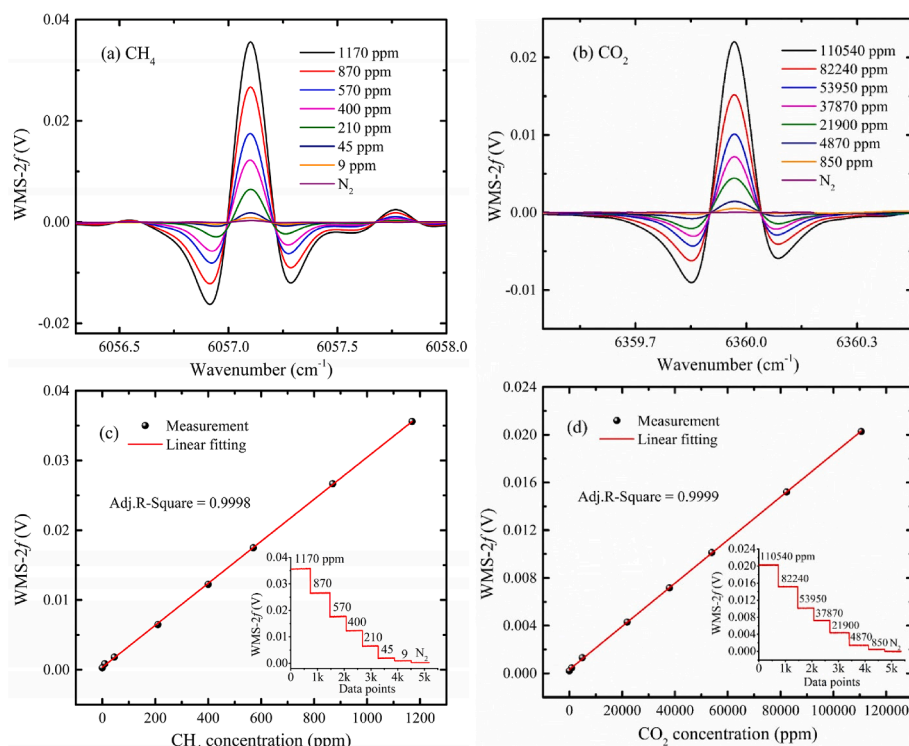


Fig. 5. Simultaneously recorded WMS-2f spectra of (a) CH<sub>4</sub> and (b) CO<sub>2</sub> at different gas concentrations, along with their corresponding linear calibration presented in (c) and (d), respectively.

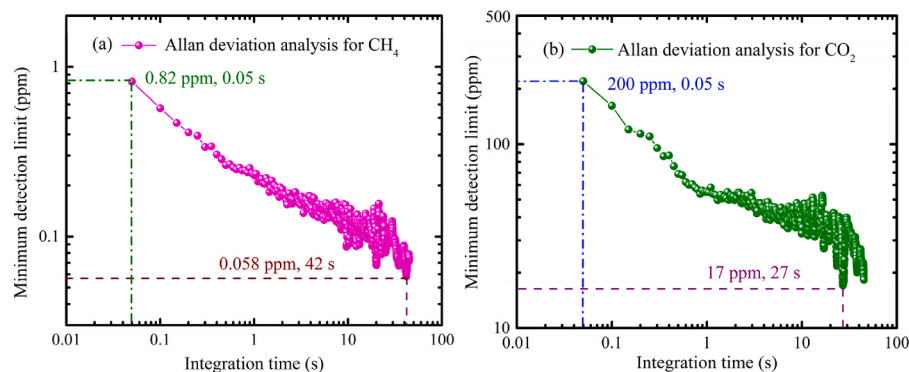


Fig. 6. Allan deviation plot for (a) CH<sub>4</sub> and (b) CO<sub>2</sub> as a function of integration time.

various peat moisture contents and at a constant airflow velocity of 27 mm/s. As the moisture content is increased, both the CH<sub>4</sub> and CO<sub>2</sub> emissions decrease significantly. This is partly attributed to the added water decreasing the dry mass of fuel and the swelling of the sample volume (decreasing dry peat bulk density with MC) [38].

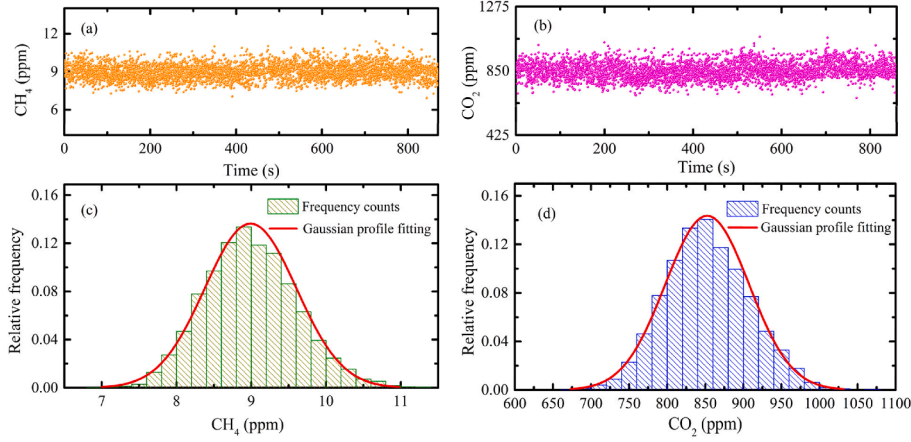
#### 4.3. Smoldering emission characteristics

Fig. 11 shows the peak and average CH<sub>4</sub>/CO<sub>2</sub> ratios under different peat moisture contents and airflow velocities. It is important to highlight that measuring the concentration of a single gas is ineffective since it greatly depends on the location of measurement. However, utilizing the ratio of two gases can circumvent this issue according to the recent work by Wang et al. [39] and Chen et al. [40] by measuring the ratio of CH<sub>4</sub> (or VOCs) to CO<sub>2</sub> to quantify smoldering emissions. Therefore, we adopt the similar strategy by studying the CH<sub>4</sub>/CO<sub>2</sub> ratio in this paper to avoid the influence of measurement location. The CH<sub>4</sub>/CO<sub>2</sub> ratio helps characterize the competition between pyrolysis and oxidation reactions in

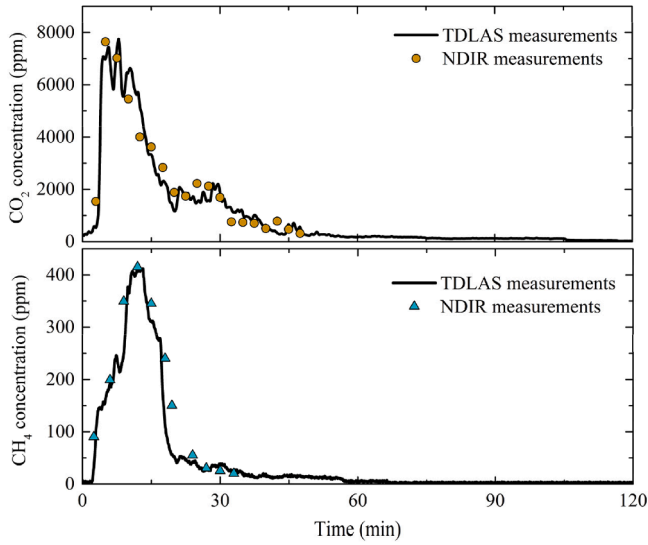
smoldering combustion. As the pyrolysis of biomass generates more CH<sub>4</sub> than the oxidation of biomass and chars [8,9,41], an increased value of CH<sub>4</sub>/CO<sub>2</sub> indicates the enhanced pyrolysis process or the weaker char oxidation.

As seen in Fig. 11(a), the average and peak CH<sub>4</sub>/CO<sub>2</sub> ratios are generally lower than 0.08 and 0.15, respectively, under all tested conditions. Specifically, it is observed that the average CH<sub>4</sub>/CO<sub>2</sub> ratio decreases from 0.06 to 0.043 as peat moisture content increases from 8% (dry peat) to 100%. As most of the CH<sub>4</sub> is produced in fuel pyrolysis [8,9,41], a higher fuel moisture content weakens the pyrolysis process thus reducing the CH<sub>4</sub> emission. On the other hand, the ratio of average CH<sub>4</sub>/CO<sub>2</sub> increases with the oxygen supply from 0.053 (10 mm/s) to 0.075 (24 mm/s), because the stronger char oxidation increases the temperature and intensity of pyrolysis reactions.

CO<sub>2</sub> and CH<sub>4</sub> are two major GHGs emitted from peat smoldering fires [3]. Although N<sub>2</sub>O is also regarded as a potent GHG, its amount from peat smoldering is very small which can be ignored here. Although CH<sub>4</sub> emission is found to be much smaller than CO<sub>2</sub>, its global warming



**Fig. 7.** Simultaneous continuous measurements of (a) 9 ppm CH<sub>4</sub> and (b) 850 ppm CO<sub>2</sub>. The corresponding frequency distribution of (c) 9 ppm CH<sub>4</sub> and (d) 850 ppm CO<sub>2</sub> measurement is plotted along with the Gaussian fitting.



**Fig. 8.** Evolution of CO<sub>2</sub> and CH<sub>4</sub> concentrations at  $u_{air} = 10$  mm/s.

effects cannot be ignored. Herein, the GHGs from peat smoldering are simplified as a mixture of CO<sub>2</sub> and CH<sub>4</sub>, and the equivalent GHG flux is estimated by [42]:

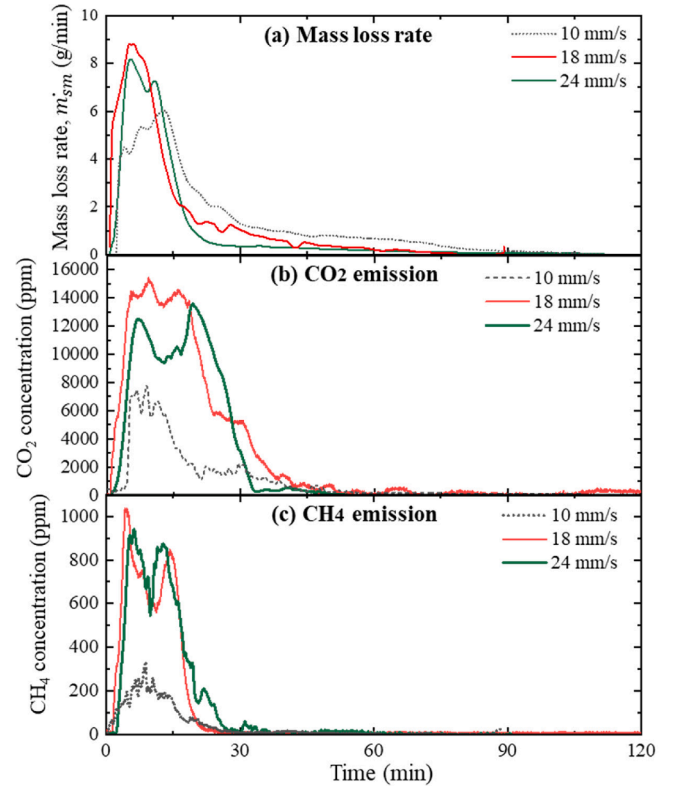
$$\dot{m}_{GHG}'' = \frac{GWP_{CO_2} \Delta \dot{m}_{CO_2}'' + GWP_{CH_4} \Delta \dot{m}_{CH_4}''}{GWP_{CO_2}} \quad (5)$$

where  $GWP$  is the global warming potential of the species. In practice, CO<sub>2</sub> is taken as the reference gas and given a 100-year  $GWP$  of 1, and  $GWP_{CH_4}$  is defined as 25 here [42]. Then,  $\dot{m}_{CO_2}''$  and  $\dot{m}_{CH_4}''$  are the emission fluxes of CO<sub>2</sub> and CH<sub>4</sub>, which can be expressed as:

$$\dot{m}_i'' = \frac{\rho_i \Delta X_i \dot{V} \times 10^{-3}}{A} \quad (6)$$

where  $\rho_i$  is the density of gas species  $i$  (kg/m<sup>3</sup>),  $\Delta X_i$  is the real-time concentration of the species  $i$  (ppm),  $\dot{V}$  is the volume flow rate in the sampling duct, which is measured to be  $1.7 \times 10^{-3}$  m<sup>3</sup>/s, and  $A$  is the cross-sectional area of the smoldering burner (m<sup>2</sup>).

Fig. 12 (a) and (b) show the time-averaged  $\dot{m}_{CO_2}''$  and  $\dot{m}_{CH_4}''$  and the equivalent  $\dot{m}_{GHG}''$  under different peat moisture contents and airflow rates, respectively. Both the moisture content and the airflow velocity have significant effects on the GHG flux. As expected, the equivalent



**Fig. 9.** Evolutions of the mass-loss rate, detected CH<sub>4</sub> and CO<sub>2</sub> emissions from dried peat smoldering under different airflow velocities.

$\dot{m}_{GHG}''$  decreases as the fuel moisture content increases, but it increases with the airflow velocity. For instance, the equivalent  $\dot{m}_{GHG}''$  is 1.5 g/m<sup>2</sup>·s under the airflow velocity of 10 mm/s, and it increases to about 3.4 g/m<sup>2</sup>·s when the airflow velocity increases to 24 mm/s.

The average emission factor ( $EF_{av}$ , g/kg) for gas species is further calculated through Eq. (7) and shown in Fig. 12 (c):

$$EF_{av}(t) = \frac{\dot{m}_{i-av}''}{\dot{m}_{sm-av}''} \times 10^3 \quad (7)$$

where  $\dot{m}_{sm-av}''$  (g/m<sup>2</sup>·s) is the average smoldering flux (mass loss rate per unit area of the fuel), and  $\dot{m}_{i-av}''$  (g/m<sup>2</sup>·s) is the average emission flux of gas species  $i$  shown in Fig. 12 (b). As shown in Fig. 12 (c), the average

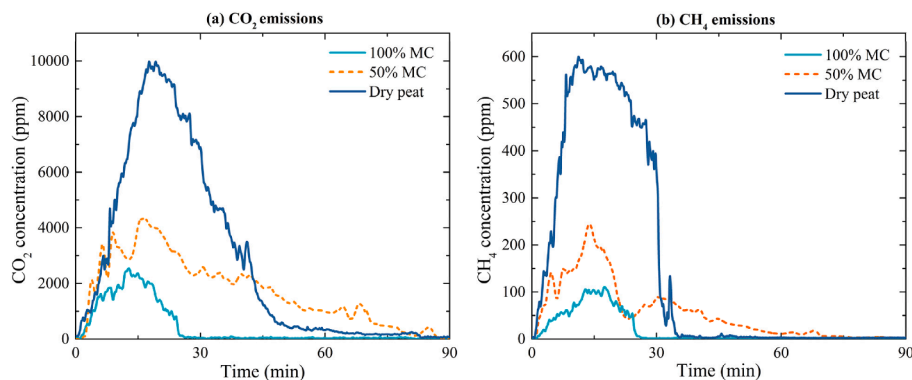


Fig. 10. Measured emissions of (a)  $\text{CO}_2$  and (b)  $\text{CH}_4$  under different peat moisture contents ( $u_{\text{air}} = 27 \text{ mm/s}$ ).

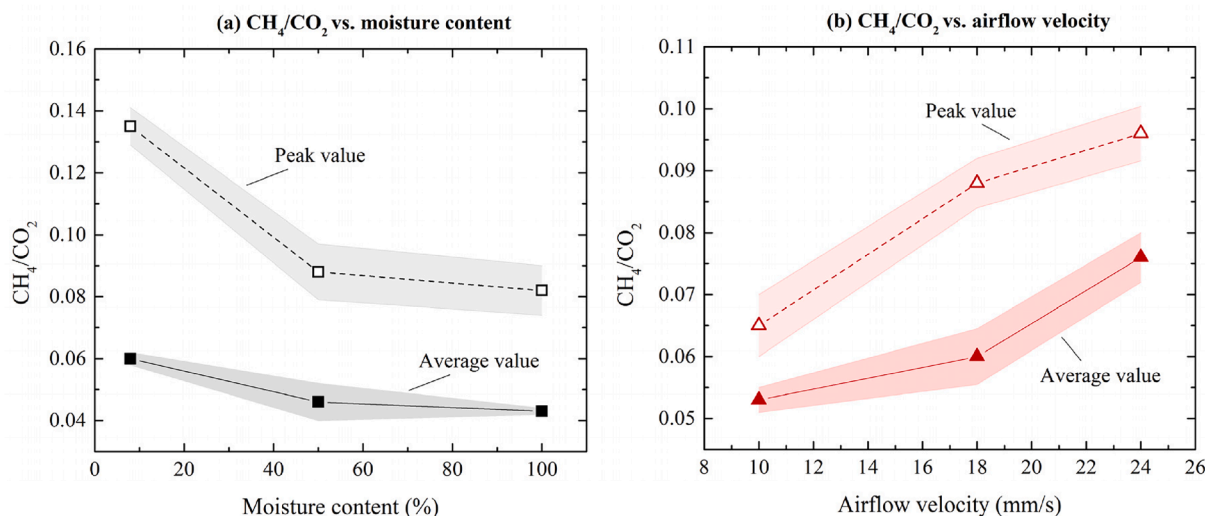


Fig. 11. Variation of  $\text{CH}_4/\text{CO}_2$  ratio with (a) peat moisture content and (b) supplied airflow velocity. The clouds represent the uncertainty of repeated tests.

EFs of  $\text{CH}_4$  are around  $20 \text{ g/kg}$  and increase with the airflow velocity. Comparatively, the average EFs of  $\text{CO}_2$  and equivalent GHGs are significantly larger than that of  $\text{CH}_4$ . When the airflow velocity rises from  $10 \text{ mm/s}$  to  $18 \text{ mm/s}$ , the EF of GHG increases from  $1008$  to  $1458 \text{ g/kg}$ . But when the airflow velocity continues to increase to  $24 \text{ mm/s}$ , the EF of GHG increases slightly to about  $1582 \text{ g/kg}$ . Therefore, it can be concluded that the GHGs emitted from smoldering wildfires are significantly influenced by fuel and environmental conditions such as the weather, climate (dry or wet season), and the wind.

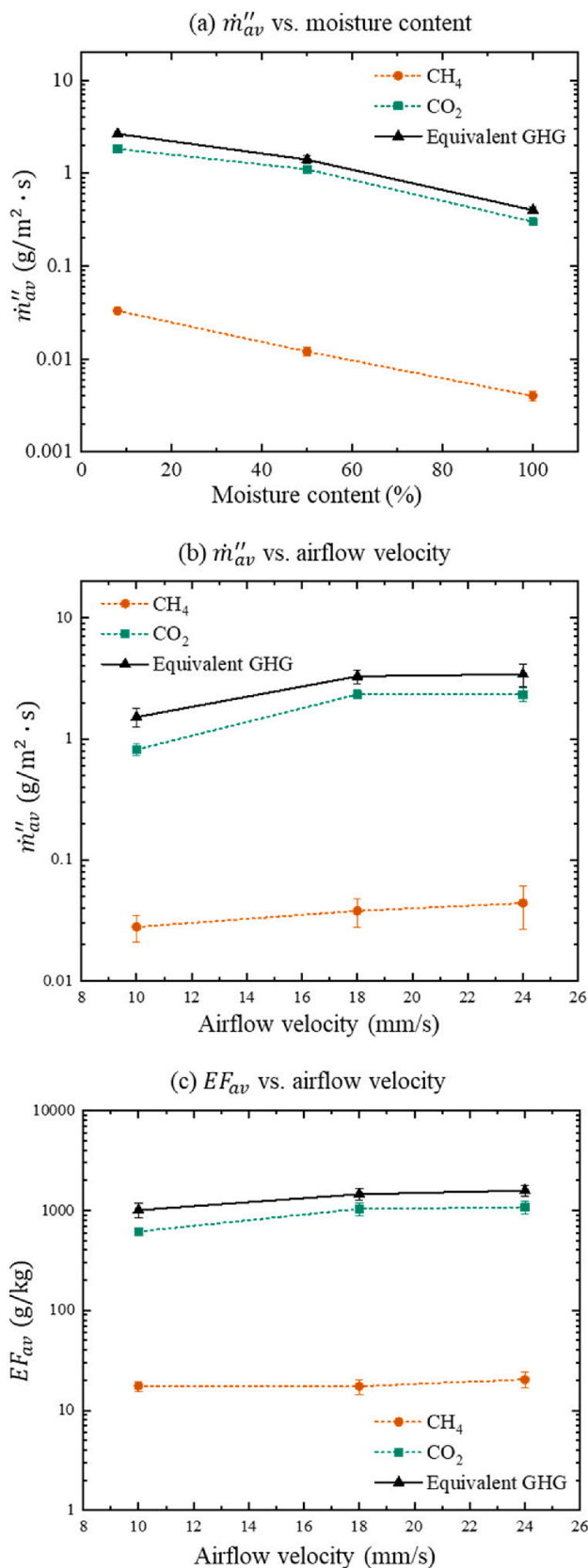
In summary, the detailed investigation discloses the capability of the developed dual-gas TDLAS sensor for simultaneously detecting  $\text{CH}_4$  and  $\text{CO}_2$  under various smoldering conditions. The TDLAS sensor has a promising potential to be used in smoldering fire detection and smoldering research to examine transient phenomena due to its superior time response.

## 5. Conclusions

A dual-gas optical sensor was developed using time-division multiplexed scanned wavelength modulation spectroscopy for peat fire detection by simultaneously measuring transient  $\text{CH}_4$  and  $\text{CO}_2$  emissions from a lab-scale smoldering peat combustion reactor. The sensor comprises two infrared lasers, an infrared photodetector, and a custom-designed Herriot multipass gas cell ( $10.3 \text{ m}$  path length). Two infrared lasers operating at  $1650 \text{ nm}$  and  $1572 \text{ nm}$  were combined for exploiting  $\text{CH}_4$  and  $\text{CO}_2$  absorption lines centered at  $6057.09 \text{ cm}^{-1}$  and  $6359.96 \text{ cm}^{-1}$ , respectively. The injection current of  $1572 \text{ nm}$  and  $1650 \text{ nm}$  lasers

was sinusoidally modulated at  $15 \text{ kHz}$  and  $18 \text{ kHz}$  with triangular scanned across the selected absorption lines of  $\text{CH}_4$  and  $\text{CO}_2$  at  $10 \text{ Hz}$ . A compact custom-designed Herriot multipass gas cell with an effective path length of  $10.3 \text{ m}$  in a volume of  $40.5 \text{ mL}$  was employed to improve detection sensitivity. Allan-Werle deviation analysis yielded the MDL of  $0.058 \text{ ppm}$  for  $\text{CH}_4$  and  $17 \text{ ppm}$  for  $\text{CO}_2$  at an optimum integration time of  $42\text{-s}$  and  $27\text{-s}$ , respectively. The simultaneous real-time measurements were recorded at an interval of  $0.1 \text{ s}$  to capture the transient  $\text{CH}_4$  and  $\text{CO}_2$  emissions under various smoldering peat fire conditions in a top-open cylinder reactor. The results agree well with the traditional commercial NDIR  $\text{CO}_2$  and  $\text{CH}_4$  analyzers. However, these commercial instruments show a slow time resolution of  $\sim 2.5 \text{ min}$  and  $\sim 3 \text{ min}$ , respectively, which is inadequate for measuring the transient change in peat fire emissions. The GHG flux and  $\text{CH}_4/\text{CO}_2$  ratio increase from  $1.5 \text{ g/m}^2 \text{ s}$  to  $3.4 \text{ g/m}^2 \text{ s}$  and  $0.053$  to  $0.075$ , respectively, with increasing oxygen supplies from  $10 \text{ mm/s}$  to  $24 \text{ mm/s}$ . However, the GHG flux and  $\text{CH}_4/\text{CO}_2$  ratio decreased from  $2.6 \text{ g/m}^2 \text{ s}$  to  $0.4 \text{ g/m}^2 \text{ s}$  and  $0.06$  to  $0.043$  with the peat moisture content increased from  $8\%$  (dry peat) to  $100\%$ . The demonstrated time-division multiplexed dual-gas sensor offers a fast temporal resolution, high sensitivity, hardware simplicity, and compactness, which make it attractive for detecting transient emissions in underground peatland fires and monitoring overall GHG emissions from smoldering wildfires. Together with the state-of-the-art  $\text{N}_2\text{O}$  optical detector [43], future work will involve the simultaneous detection of the top three primary GHGs from smoldering biomass combustion.





**Fig. 12.** Average equivalent GHG flux from peat smoldering versus (a) moisture content and (b) airflow velocity and (c) the average emission factors. The error bars ( $SE = \sigma/\sqrt{n}$ , where  $n = 2$ ) shows the experimental uncertainty.

## CRediT authorship contribution statement

**Mohsin Raza:** Conceptualization, Methodology, Investigation, Formal analysis, Validation, Visualization, Writing – original draft, Writing – review & editing. **Yuying Chen:** Methodology, Investigation, Formal analysis, Validation, Visualization, Writing – original draft, Writing – review & editing. **Joshua Trapp:** Methodology, Investigation. **Haojia Sun:** Methodology, Investigation. **Xinyan Huang:** Conceptualization, Methodology, Supervision, Writing – review & editing, Project administration, Funding acquisition. **Wei Ren:** Conceptualization, Methodology, Formal analysis, Validation, Visualization, Writing – review & editing, Supervision, Project administration, Funding acquisition.

## Declaration of Competing Interest

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

## Data availability

Data will be made available on request.

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